## How to determine the total head

## 1. Formula for calculating the total head



Fig. 1 Positive suction type


Fig. 2 Negative suction type


Fig. 3

- Total head P6-(P1-P2) $=$ P2 + P3 + P4 + P5-P1
$\mathrm{P} 1=$ positive suction $(+)$
negative suction (-)

P1: Height difference between water level of the receiving tank and water supply unit
P2: Pressure loss of the water supply pipe and water supply apparatus on the suction pipe side of the water supply unit
P3: Pressure loss of the water supply pipe and water supply apparatus on the discharge pipe side of the water supply unit
P4: Pressure required to use the water supply apparatus at the highest end
P5: Actual pump head (head difference between the water supply unit and the water supply apparatus at the highest end)
$P 6$ : Discharge pressure of the water supply unit $P 6=P 3+P 4+P 5$

- Total head ${ }^{* 1} \mathrm{P} 7-\mathrm{P} 8=(\mathrm{P} 1+\mathrm{P} 2+\mathrm{P} 3+\mathrm{P} 4+\mathrm{P} 5+\mathrm{P} 6)-\mathrm{P} 0$

P 0 : Water distribution pipe water pressure
P1: Height difference between the water distribution pipe and the direct connecting booster pump unit
P2: Head loss of the water supply pipe and water supply apparatus on the suction side of the direct connecting booster pump unit
P3: Head loss of the direct connecting booster pump unit (loss by backflow preventer) ${ }^{* 2}$
P4: Head loss of water supply pipes and water supply apparatus on the discharge side of the direct connecting booster pump unit
P5: Pressure required to use the water supply apparatus at the highest end
P6: Height difference between the direct connecting booster pump unit and the water supply apparatus at the highest end
P7: Discharge pressure of the direct connecting booster pump unit
P8: Pump suction side effective pressure
NOTE) *1 The total pump head indicates what was pressurized by direct connecting booster pump unit. *2 P3 is the sum of the loss by backflow preventer and loss in the unit. In our selection diagram, the performance is displayed after subtracting the loss in the unit, so only the loss by backflow preventer is shown
2. Materials related to total pump head calculation
(1) Minimum required pressure for water supply equipment

Table 1 Minimum required pressure for instruments

| Name of fixtures | Required pressure (when flowing) [kPa] |
| :---: | :---: |
| Generall faucet | 30 |
| Lavatory flushing valve * | 70 |
| Urinal faucet | 30 |
| Urinal flush valve | 70 |
| Shower | 70 |
| Instantaneous gas water heater |  |
| No. 4-5 | 40 |
| No. 7-16 | 50 |
| No. 22-30 | 80 |

Note * Same for tankless lavatory
Cited Document: The Society of Heating, Air-Conditioning and Sanitary Engineers of Japan: Handbook of Heating, Air-Conditioning and Sanitary Engineering, 14th edition
(2) Pressure loss

Pressure loss includes pressure loss at the inlet and outlet of pipes, pressure loss due to pipe friction, pressure loss due to water meters and water supply apparatus, pressure loss due to bending, branching, and cross-sectional change of the pipe. Major items of these are friction pressure loss of pipes, pressure loss due to water meters and water supply apparatus, and others can be omitted in calculation because they have little effect.

- Determination of water supply pipe diameter

Determine the pipe diameter used to calculate the pressure loss. The diameter of the water supply pipe is determined based on the flow diagram (Fig. 4 to Fig.7) according to the piping material used in accordance with the limits of the instantaneous maximum water supply and flow velocity. Generally, the flow rate should be kept below $2 \mathrm{~m} / \mathrm{s}$ because too high a flow rate can cause flow sound or water hammer.

- How to determine the pressure loss

Calculate the equivalent pipe length using "A. Pressure loss of joints and valves" and add the actual total straight pipe length to the sum of the values to obtain the total equivalent pipe length. Multiply this by the pressure loss per unit length of various piping according to "B. Pressure loss of piping (flow rate diagram (Fig. 4 to Fig.7)" to get the total pressure loss.

Many types of joints and valves are used in the water supply system, and it is very complicated to calculate the pressure loss due to these joints and valves one by one. Therefore, the pressure loss due to joints and valves is calculated by replacing the pressure loss of straight pipes which corresponds to the pressure loss of straight pipes of the same diameter.

## A. Pressure loss of joints and valves

Table 2 Equivalent pipe lengths of joints and valves (for steel pipes and stainless steel pipes)

| Nominal diameter |  | Equivalent pipe length [m] |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| A | Su | $90^{\circ}$ elbow | $45^{\circ}$ elbow | $9^{\circ}{ }^{\circ}$ t tube (shunt) | $90^{\circ} \mathrm{T}$ tube (Direct Current) | Gate valve*1 | Ball valve*1 | Angle valve, foot valve swing type check valve*2 | Socket |
| 13 | 13 | 0.30 | 0.18 | 0.45 | 0.09 | 0.06 | 2.27 | 2.4 | 0.09 |
| 20 | 20 | 0.38 | 0.23 | 0.61 | 0.12 | 0.08 | 3.03 | 3.6 | 0.12 |
| 25 | 25 | 0.45 | 0.30 | 0.76 | 0.14 | 0.09 | 3.79 | 4.5 | 0.14 |
| 32 | 40 | 0.61 | 0.36 | 0.91 | 0.18 | 0.12 | 5.45 | 5.4 | 0.18 |
| 40 | 50 | 0.76 | 0.45 | 1.06 | 0.24 | 0.15 | 6.97 | 6.8 | 0.24 |
| 50 | 60 | 1.06 | 0.61 | 1.52 | 0.30 | 0.21 | 8.48 | 8.4 | 0.30 |
| 65 | 75 | 1.21 | 0.76 | 1.82 | 0.39 | 0.24 | 10.00 | 10.2 | 0.39 |
| 80 | 80 | 1.52 | 0.91 | 2.27 | 0.45 | 0.30 | 12.12 | 12.0 | 0.45 |
| 100 | 100 | 2.12 | 1.21 | 3.18 | 0.61 | 0.42 | 19.09 | 16.5 | 0.61 |
| 120 | 125 | 2.73 | 1.52 | 3.94 | 0.76 | 0.52 | 21.21 | 21.0 | 0.76 |
| 150 | 150 | 3.03 | 1.82 | 4.55 | 0.91 | 0.61 | 25.45 | 21.0 | 0.91 |
| 200 | 200 |  |  |  |  |  |  | 33.0 |  |
| 250 | 250 |  |  |  |  |  |  | 43.0 |  |

NOTE For stainless steel pipes for general piping, this table is used because there is no specific data.
*1 Bronze castings
*2 50A or less: bronze casting, 65A or more: cast iron

Table 3 Equivalent pipe lengths of pipe joints and valves (rigid vinyl chloride lined steel pipe for water supply)

| Nominal diameter | Equivalent pipe length [m] |  |  |  |  |  |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Nominal diameter [mm] | $90^{\circ}$ elbow | $45^{\circ}$ elbow | $90^{\circ} \mathrm{T}$ <br> (Branch flow) | $90^{\circ} \mathrm{T}$ <br> (Straight flow) | Gate valve | Ball valve | Angle valve | Check valve |
| 15 | 3.0*1 | 2.3*1 | 3.8*1 | $1.2 * 1$ | 3.5*2 | 4.5 | 2.4 | 5.5*2 |
| 20 | $3.1 * 1$ | $2.2 * 1$ | $3.8 * 1$ | $1.6 * 1$ | $2.3 * 2$ | 6.0 | 3.6 | $2.7 * 2$ |
| 25 | $3.2 * 1$ | 1.8*1 | $3.3 * 1$ | $1.2 * 1$ | $1.7 * 2$ | 7.5 | 4.5 | 2.9*2 |
| 32 | 3.6*1 | 2.3*1 | 4.0*1 | $1.4 * 1$ | $1.3 * 2$ | 10.5 | 5.4 | $3.2 * 2$ |
| 40 | $3.3 * 1$ | 1.9*1 | $3.6 * 1$ | $0.9 * 1$ | $1.7 * 2$ | 13.5 | 6.6 | 2.6*2 |
| 50 | $3.3 * 1$ | 1.9*1 | $3.5 * 1$ | $0.9 * 1$ | 1.9*2 | 16.5 | 8.4 | $3.7 * 2$ |
| 65 | 4.4*1 | 2.4*1 | 4.4*1 | 1.1*1 | 0.48 | 19.5 | 10.2 | 4.6 |
| 80 | 4.6*1 | 2.4*1 | 4.9*1 | 1.3*1 | 0.63 | 24.0 | 12.0 | 5.7 |
| 100 | $4.7 * 1,4.2$ | $2.7 * 1,2.4$ | $6.6^{* 1}, 6.3$ | $1.5^{* 1}, 1.2$ | 0.81 | 37.5 | 16.5 | 7.6 |
| 125 | 5.1 | 3.0 | 7.5 | 1.5 | 0.99 | 42.0 | 21.0 | 10.0 |
| 150 | 6.0 | 3.6 | 9.0 | 1.8 | 1.20 | 49.5 | 24.0 | 12.0 |
| 200 | 6.5 | 3.7 | 14.0 | 4.0 | 1.40 | 70.0 | 33.0 | 15.0 |
| 250 | 8.0 | 4.2 | 20.0 | 5.0 | 1.70 | 90.0 | 43.0 | 19.0 |

Note 1) The foot valve is the same as the angle valve, and the check valve is the swing type.
2) Use the data for steel pipes for data without *2.
*1 Pipe end anti-corrosion type, according to the Japan Pipe Fittings Association data.
*2 Pipe end anti-corrosion type, according to the data by K Company and Y Company.

## B. Piping pressure loss

Calculate the pressure loss per unit length of various piping.
Hazen-Williams equations are commonly used in water supply facilities. In addition, the Weston equation is said to fit well with pipes of 50 mm or less, and is applied in the case of the direct connection method of water supply. Calculate the pressure loss per unit length using the flow rate diagram (Fig. 4 to Fig. 7) for each type of piping based on the Hazen-Williams equation.

Table 4 Flow coefficients of various pipes

| Pipe type | C |
| :--- | :---: |
| New brass pipes, new copper pipes, new lead pipes, new cement lined <br> cast iron pipes or steel pipes, new asbestos cement pipes | 140 |
| New steel pipes, new cast iron pipes, old brass pipes, old copper pipes, <br> rigid polyvinyl chloride pipes | 130 |
| Old cement lining pipes, ceramic pipes | 110 |
| Old cast iron pipes, old steel pipes | 100 |

1) Hazen-Williams equation

$$
\begin{aligned}
& H=10.666 \cdot C^{-1.85} \cdot D^{-4.87} \cdot Q^{1.85} \cdot L \\
& V=\left.0.35464 \cdot C \cdot D^{0.63} \cdot\right|^{0.54} \\
& Q=\left.0.27853 \cdot C \cdot D^{2.63} \cdot\right|^{0.54}
\end{aligned}
$$

2) Weston's equation
$H=\left(0.0126+(0.01739-0.1087 D) / N^{0.5}\right)(L / D)\left(V^{2} / 2 g\right)$
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H: Friction pressure loss (m) for length L (m)
C: Flow rate coefficient (see Table 10)
D: Pipe inner diameter (m)
Q: Flow rate (m}\mp@subsup{}{}{3}/\textrm{s}
L : Length of pipe (m)
V : Average flow velocity in tube (m/s)
I = H/L: hydraulic gradient
g : Gravitational acceleration (9. 8m/s)
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Fig. 4 Flow rate diagram of carbon-steel pipe (JIS G 3452) for pipes (HAS-S 206-1982)


Fig. 6 Flow rate diagram of rigid vinyl chloride pipe (SHASE-S 206-2009)


Fig. 5 Flow rate diagram of stainless-steel pipe for ordinary pipes (SHASE-S 206-2009)


Fig. 7 Flow rate diagram of rigid vinyl chloride lined steel pipe (SHASE-S 206-2009)

